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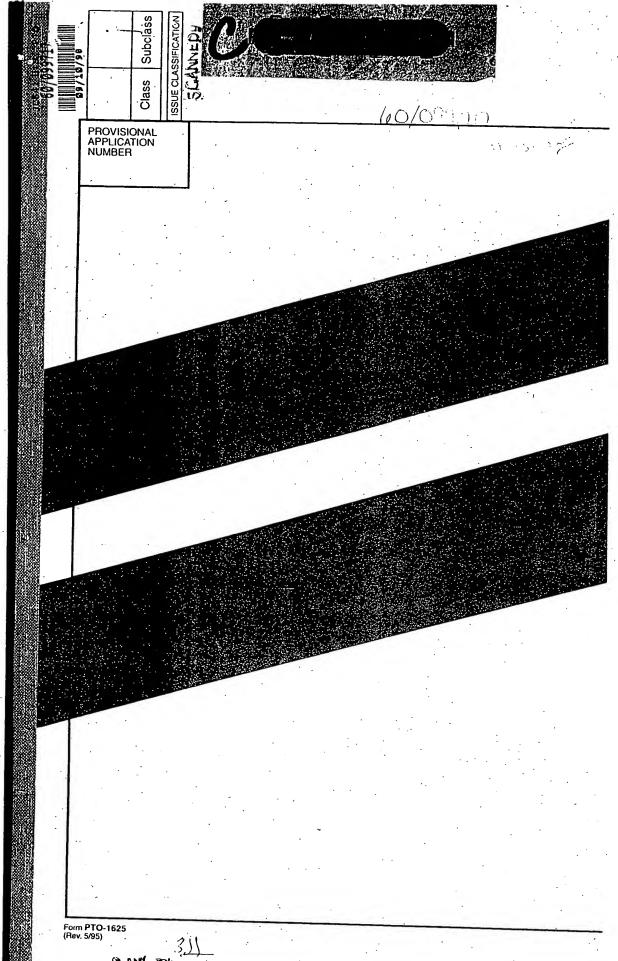
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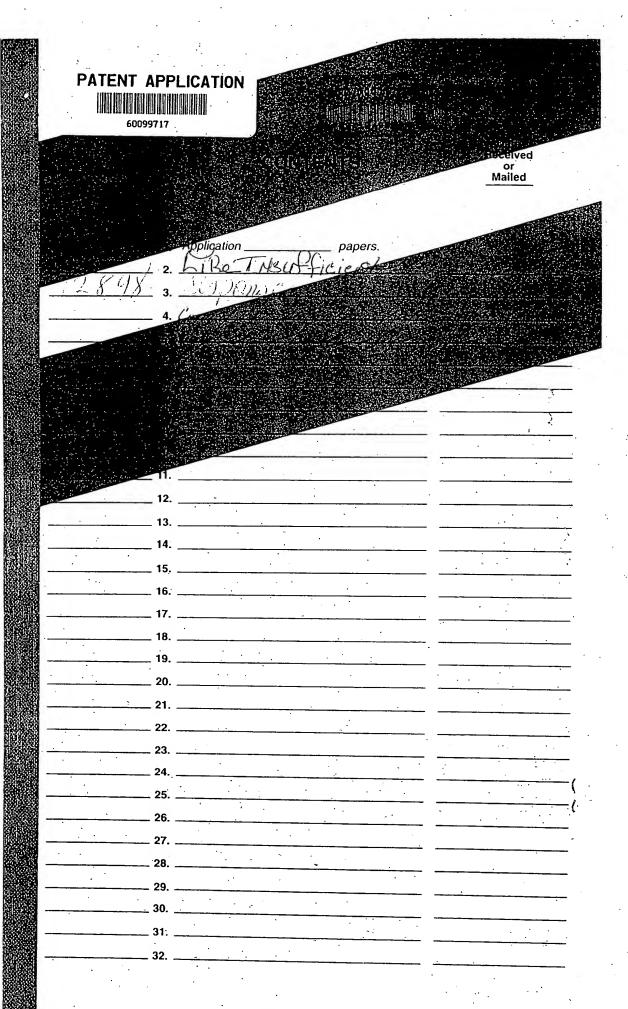
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PATENT	APPLICATION	SERIAL	NO.	

U.S. DEPARTMENT OF COMMERCE PATENT AND TRADEMARK OFFICE FEE RECORD SHEET

09/16/1998 BHINES 00000013 60099717

01 FC:114 75.00 OP

Adjustment date: 03/08/1999 NTRAN1
09/16/1998 BHINES 00000013 60099717
01 FC:114 75.00 OP

PTO-1556 (5/87) Refund Ref: 04/1999 HTROM1 0000078724

CHANGE OF ADDRESS/POWER OF ATTORNEY

LOCATION 9200 SERIAL NUMBER 60099717 PATENT NUMBER

THE CORRESPONDENCE ADDRESS HAS BEEN CHANGED TO CUSTOMER # 22442

THE PRACTITIONERS OF RECORD HAVE BEEN CHANGED TO CUSTOMER # 22442

THE FEE ADDRESS HAS BEEN CHANGED TO CUSTOMER # 22442

ON 12/14/99 THE ADDRESS OF RECORD FOR CUSTOMER NUMBER 22442 IS:

SHERIDAN ROSS PC 1560 BROADWAY SUITE 1200 DENVER CO 80202

AND THE PRACTITIONERS OF RECORD FOR CUSTOMER NUMBER 22442 ARE:

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SERIAL NUMBER		FILING DATE	CLASS	GROU	JP ART UNIT	ATTORNEY DOC	KET NO.	
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METHOD OF REMOVING ORGANIC LIXIVIANT FROM COPPER 8X-EW ELECTROLYTE STREAM"

The present invention relates generally to leaching systems and specifically to treatment systems for removing an organic lixiviant from a leaching solution.

THE PROBLEM

The present invention generally relates to the removal of copper ions from copper ore, and more particularly to enhanced removal of copper ions using a microfiltration or ultrafiltration process which removes entrained organic from the aqueous rich electrolyte solution before it enters the electrowin tankhouse. This process improves the copper hydrometallurgical mining process through more efficient copper electrowinning.

The techniques used to remove copper from raw ore determine the overall efficiency of the copper mining operation. Hydrometallurgical copper mining operations using a leaching system and a copper extraction plant, such as a solvent extraction/electrowinning (SX/EW) plant, are now accepted processes in the copper mining industry. Currently, electrowon copper accounts for about 30% of total U.S. copper production. Worldwide, there are more than 26 major heap, dump, or in-situ leaching operations using SX/EW, with a total capacity of 7800,000 tons of copper annually. The industry trend continues towards this

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technology as higher-grade ores are depleted and smelting costs increase. Other advantages of this technology, such as the ability to process low-grade ores, low labor requirements, ease of operation in remote areas, and low operating costs, make it attractive to mining companies.

"Copper hydrometallurgy", in which copper ions are leached or otherwise extracted from raw ore using liquid chemical agents, has been of interest since as early as the 17th century when copper recovery methods involving iron precipitating agents from sulfuric acid based copper solutions were tested. The hydrometallurgical circuit consists of copper leaching and copper recovery.

First, a copper leaching agent, "lixiviant", is selected for use in leaching copper ions from copper ore. Representative lixiviants include but are not limited to sulfuric acid (H₂SO₄), a combination of H₂SO₄ and ferric sulfate, Fe₂(SO₄)₃ (primarily for sulfide containing ore materials), acidic chloride solutions (e.g. ferric chloride, FeCl₂) or cupric chloride, CuCl, nitrate solutions, ammonia, and ammonium salt compositions. Sulfuric acid is by far the most common lixiviant. The lixiviant is applied to the ore (which is stacked or piled in a large heap or dump) via a sprinkler type system and allowed to percolate downwardly into the ore. As a result, copper ions are leached from the ore and collected within the lixiviant to generate a lixiviant product that consists of a copper ion

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concentration (also known as a "pregnant leach solution").

The lixiviant exits the bottom of the ore and is collected.

Further information regarding the lixiviant leaching process is disclosed in U.S. Patent No. 5,476,591 to Green et al., which is incorporated herein by reference.

Next, a copper recovery process is used to selectively extract copper from the collected lixiviant. Representative copper recovery processes include but are not limited to solvent extraction/electrowin (SX/EW), direct electrowinning, ion exchange-electrowin (IX/EW), and iron precipitation. Solvent extraction/electrowin is presently the most common copper recovery process. SX/EW technology was implemented in the 1960s with the development of special organic extractants for copper. The SX/EW process consists

of three closed solution loops. In the first loop, the acid

multitude of other metal ions is fed into a mixer/settler

tank where it is contacted with a copper-extracting organic

liquid, commonly referred to as "lix". The "lix"

preferentially extracts from 70 to 90% of the copper ions from the acid leaching feed solution. The second closed loop extraction step involves contacting the loaded organic with an electrolyte stream from the electrowinning process.

The copper ions are transferred from the organic solution or

leach solution containing valuable copper ions and a

25 "lix" to the lean electrolyte. In the third and final closed loop, the rich electrolyte flows between a cathode

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plate and an insoluble anode, where 70-90% of the copper is removed through "plating". The electrochemical cell "plates" a stainless steel electrode with copper using an applied current. The copper plated cathode plates are then periodically removed from the process to obtain the solid, high purity copper product.

The copper electrowinning "EW" process must be improved to overcome inherent problems such low current efficiency, poor copper product quality, and poor copper removal from the stainless steel cathode electrode. The present invention specifically provides an improved method for copper recovery in which the entrained organic in the rich electrolyte is removed with a membrane system, leaving an organic - free rich electrolyte for superior copper electrowinning. The direct result of organic removal with the membrane process is better copper product quality. Accordingly, the invention represents an advance in the art of copper mining technology, as described in detail herein.

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SUMMARY OF THE INVENTION

These and other needs are met by the process of the present invention which recovers a metal from a metal-containing material. The process includes the steps of:

- (a) contacting a metal leaching agent with the metal-containing material to solubilize the metal in a pregnant leach solution;
 - (b) contacting the pregnant leach solution with an organic collector to transfer at least a portion of the solubilized metal to the organic collector to form a pregnant organic solution including a metal-containing organic collector and a stripped pregnant leach solution, wherein the stripped pregnant leach solution may contain at least a portion of the organic collector;
 - (c) contacting the pregnant organic solution with an electrolyte (or catholyte) solution to form a stripped pregnant organic solution comprising most of the organic collector and a pregnant electrolyte (or catholyte) solution comprising at least most of the copper and some of the organic collector;
 - (d) filtering the pregnant electrolyte (or catholyte) solution with a filter to form a concentrate containing at least most of the organic collector and a permeate; and
 - (e) recovering the metal from the permeate.

The process can further include the steps of recycling the concentrate to steps (b) or (c). As set forth in U.S.

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Provisional Application, "Method of Removing Organic Lixiviant from Copper SX/EW Raffinate Stream," having Attorney File No. 3376-18PROV, filed October 30, 1997, which is incorporated herein by this reference, the stripped pregnant leach solution can also be filtered to recover the organic collector.

By recovering the organic collector in the concentrate, the process can reduce, or eliminate, carry over of the organic collector into the electrowinning step and can recover the organic collector from the concentrate for reuse. The substantial absence of residual organic collector from the permeate addresses many inherent problems in copper electrowinning, including low current efficiency, poor copper product quality, and poor copper removal from the stainless steel cathode electrode. Accordingly, the process provides a large, direct economic benefit.

The metal, organic collector, and leaching agent can be a variety of materials. The metal is preferably selected from the group consisting of copper, cobalt, gold, silver, uranium, nickel and mixtures thereof. The organic collector is preferably selected from the group consisting of hydroxyphenyl oximes (aka the reagents sold under the trade names "LIX-622N," "LIX-54," "LIX 63," "ACORGA P-5100," "ACORGA M5640" and "ALAMINE 336" (uranium extraction)) and mixtures thereof. The leaching agent is preferably selected from the group consisting of sulfuric acid, a chloride, a nitrate,

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ammonia, ammonium salts, a sulfate, a cyanide, a thiocyante and mixtures thereof.

The filter is preferably a micro- or ultrafilter. The filter preferably has a pore size ranging from about 30Å (or 0.003 microns) to about 1000Å (or .01 microns) and more preferably ranging from about 50Å (or .05 microns) to about 500Å (.05 microns).

The filtration step preferably causes the concentrate to constitute less of the pregnant electrolyte (or catholyte) solution than the permeate. More preferably, the concentrate constitutes no more than about 50% and most preferably no more than about 5% of the pregnant electrolyte (or catholyte) solution. More preferably, the permeate constitutes at least about 50% and most preferably at least about 95% of the pregnant electrolyte (or catholyte) solution.

The permeate comprises at least most of the electrolyte (or catholyte) in the pregnant electrolyte (or catholyte) solution. Preferably, the permeate comprises at least about 50% and more preferably at least about 95% of the electrolyte (or catholyte) in the pregnant electrolyte solution.

The concentrate comprises at least most of the organic collector in the pregnant electrolyte (or catholyte) solution. Preferably, the concentrate comprises at least about 95% and more preferably at least about 99% of the

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organic collector in the pregnant electrolyte (or catholyte) solution. Further details concerning the filtration step and the filter are set forth in U.S. Patents 5,476,591; 5,310,486, and 5,116,511, each of which is incorporated fully herein by reference.

BRIEF DESCRIPTION OF THE DRAWINGS

Fig. 1 is a flow schematic of a preferred embodiment of a process according to the present invention.

DETAILED DESCRIPTION OF THE INVENTION

The process improvements claimed in the present invention will result from utilizing a microfiltration or ultrafiltration membrane system to process the rich electrolyte before it enters the electrowin tankhouse.

As illustrated by Figure 1, a strong sulfuric acid solution 4 passes downwardly through a heap or dump 8 of low-grade copper ore and a liquid product 12 is produced which contains remaining amounts of acid in combination with metal ions. In a first loop 16, the liquid product 12 containing copper ions and other dissolved metals is fed to a mixer/settler tank 20 where it is contacted with an organic material (e.g., a lix). The organic material forms compounds with the copper ions. The mixture forms two phases—an organic phase and an inorganic phase. The organic phase is removed to form the organic solvent 24.

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The inorganic phase is removed to form the acid leach solution 28. In a second loop 32, the organic solvent 24 is contacted in a mixer/settler tank 36 with an electrolyte stream 40 from the electrowinning circuit. The copper ions are transferred from the organic solvent 24 to the electrolyte stream 40. The resulting mixture forms two phases -- a copper lean organic solvent 44 and a copper rich electrolyte 48. The two phases are separated with the organic solvent 44 being recycled to the mixer/settler tank 20 and the copper rich electrolyte 48 being further treated for copper recovery. In a third and final closed loop 52, the copper rich electrolyte 48 exiting the mixer/settler tank 36 is passed through a microfiltration or ultrafiltration membrane system 56. The membrane system 56 separates the rich electrolyte into two streams: permeate 60 and concentrate 64. The concentrate 64 consists of substantially all the entrained organic in the electrolyte The permeate 60 consists of a substantially organicfree solution X to be sent directly to the electrowon tankhouse 68. In the electrowon tankhouse 68, the permeate or organic-free solution 60 flows between a cathode plate and an insoluble anode, where copper is removed through "plating". The electrochemical cell "plates" a stainless steel electrode with copper using an applied current. copper plated cathode plates are then periodically removed

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from the process to obtain the solid, high-purity copper product.

The concentrate 64 is sent directly back to the mixer tank 36 where the copper lean electrolyte is contacted with the copper rich organic. The organic in the membrane concentrate is reused with this method, thereby reducing organic losses. Presently, copper mining operations are trying to remove organic from the rich electrolyte by decantation, centrifuging, or coarse filtration in an attempt to maintain a high quality copper product and recover the expensive organic. For example, at one mine organic losses from the rich electrolyte are estimated at \$50,000 to \$500,000 per year. The economic loss due to derating copper quality from Grade A cathode quality is also reported as very significant by those well versed in the It is clear that using a membrane system 56 to remove the entrained organic offers significant, direct process and operating cost advantages. In addition, removal of the entrained organic prevents a serious safety problem in the electrowin tankhouse. Localized organic vapor build-up in the tankhouse has caused serious explosions at existing SX/EW facilities.

The membrane system 56 would process 100 - 10,000 gallons per minute of rich electrolyte, with 40-95% of the feed flow becoming permeate product (organic - free).

Typical microfiltration and ultrafiltration membranes used

would be MX, G, J, K, and DS-7 series elements from Osmonics/Desal of Vista, CA. These spiral wound elements use poly acrylinitril, PTFE (Teflon), PVDF, and/or polyarimid membrane materials. The described membranes span the microfiltration/ultrafiltration membrane category, with molecular weight cut-offs of 3,000 to 200,000 MWCO and pore sizes of 0.003 microns to 0.1 micron.

A typical system would process 1,000 gpm of rich electrolyte through 348 each 8 inch spiral wound JX membrane elements. The system would split the feed flow into 900 gpm of permeate 60 and 100 gpm of concentrate 64. The concentrate 64 would be returned to the mixer 36 where copper rich organic contacts copper lean electrolyte 72. The permeate 60, containing no organic, would be sent directly to the electrowin tankhouse 68.

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What is claimed is:

- A process for recovering a metal from a metalcontaining material, comprising:
- (a) contacting a metal leaching agent with the metal-containing material to solubilize the metal in a pregnant leach solution;
- (b) contacting the pregnant leach solution with an organic collector to transfer at least a portion of the solubilized metal to the organic collector to form a pregnant organic solution including a metal-containing organic collector and a striped pregnant leach solution;
- (c) contacting the pregnant organic solution with an electrolyte solution to form a stripped pregnant organic solution comprising most of the organic collector and a pregnant electrolyte solution comprising at least most of the copper and some of the organic collector;
- (d) filtering the pregnant electrolyte solution with a filter to form a concentrate containing at least most of the organic collector and a permeate; and
 - (e) recovering the metal from the permeate.
- The process of Claim 1, further comprising: recycling the concentrate to at least one of steps (b) and (c).

- 3. The process of Claim 1, further comprising:
- (e) recovering the organic collector from the concentrate.
- 4. The process of Claim 1, wherein the metal is selected from the group consisting of copper, gold, sivler, uranium, nickel and mixtures thereof.
- 5. The process of Claim 1, wherein the organic collector is selected from the group consisting of hydroxyphenyl oximes, alamines, and mixtures thereof.
- 6. The process of Claim 1, wherein the leaching agent is selected from the group consisting of sulfuric acid, a chloride, a nitrate, ammonia, ammonium salts, a sulfate, a cyanide, a thiocyanate, and mixtures thereof.
- 7. The process of Claim 1, wherein the filter has a pore size ranging from about 0.003 to about 0.1 microns.
- 8. The process of Claim 1, wherein the concentrate constitutes no more than about 50% of the pregnant electrolyte solution.

- 9. The process of Claim 1, wherein the permeate constitutes at least about 50% of the pregnant electrolyte solution.
- 10. The process of Claim 1, wherein the permeate comprises at least most of the electrolyte in the pregnant electrolyte solution.
- 11. The process of Claim 1, wherein the permeate comprises at least about 50% of the electrolyte in the pregnant electrolyte solution.
- 12. The process of Claim 1, wherein the concentrate comprises at least about 95% of the organic collector in the pregnant electrolyte solution.
- 13. The process of Claim 1, wherein the stripped pregnant leach solution contains at least a portion of the organic collector and further comprising:

filtering the stripped pregnant leach solution with a second filter to form a second concentrate containing at least most of the organic collector and a second permeate.

14. The process of Claim 13, further comprising: contacting the second permeate with metal-containing material.

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- 15. A process for recovering a metal from a metal-containing material, comprising:
- (a) contacting a pregnant metal-containing solution with an organic collector to transfer at least a portion of a solubilized metal in the pregnant metal-containing solution to the organic collector to form a pregnant organic solution including a metal-containing organic collector and a stripped solution;
- (b) contacting the pregnant organic solution with an electrolyte solution to form a stripped pregnant organic solution comprising most of the organic collector and a pregnant electrolyte solution comprising at least most of the copper and some of the organic collector;
- (c) filtering the pregnant electrolyte solution with a filter to form a concentrate containing at least most of the organic collector and a permeate; and
 - (d) recovering the metal from the permeate.

ABSTRACT

A treatment system for removing organic lixiviant from a copper electrolyte solution. An aqueous copper electrolyte stream containing entrained organic, i.e. . "rich electrolyte" from a copper extraction process, is passed through a microfiltration or ultrafiltration membrane system to produce an organic rich concentrate and an organic free permeate. The permeate is fed directly to the copper electrowin tankhouse for recovery of superior grade cathode The concentrate is returned to the mixer tank where the copper rich organic solvent and aqueous copper lean electrolyte are combined. The result of this membrane filtration of the copper electrolyte is removal of organic previously passed on to the electrowin tankhouse. organic in the rich electrolyte results in decreased current efficiency, decreased copper cathode quality, difficulty in removing the copper sheet from the stainless steel cathode, and a safety concern with the explosion potential of the organic.

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VERIFIED STATEMENT (DECLARATION) CLAIMING MALL ENTITY STATUS JAN 1 9 1999 (32 CFR 1.9(f) and 1.27(c)) - SMALL BUSINESS CONCERN

#4

I hereby declare that I am an official empowered to act on behalf of the small business concern, HW PROCESS TECHNOLOGIES, INC. of 1208 Quail Street, Lakewood, Colorado 80215.

I hereby declare that the above-identified small business concern qualifies as a small business concern as defined in 13 CFR 121.3-18, and reproduced in 37 CFR 1.9(d), for purposes of paying reduced fees under section 41(a) and (b) of Title 35, United States Code, in that the number of employees of the concern, including those of its affiliates, does not exceed 500 persons. For purposes of this statement, (1) the number of employees of the business concern is the average over the previous fiscal year of the concern of the persons employed on a full-time, part-time or temporary basis during each of the pay periods of the fiscal year, and (2) concerns are affiliates of each other when either, directly or indirectly, one concern controls or has the power to control both.

I hereby declare that rights under contract or law have been conveyed to and remain with the small business concern identified above with regard to the invention, entitled "METHOD OF REMOVING ORGANIC LIXIVIANT FROM COPPER SX-EW ELECTROLYTE STREAM" and identified as Attorney File No. 3376-21PROV2, described in application Serial No. 60/099,717, filed on September 10, 1998.

If the rights held by the above-identified small business concern are not exclusive, each individual, concern or organization having rights to the invention is listed below* and no rights to the invention are held by any person, other than the inventor, who could not qualify as a small business concern under 37 CFR 1.9(c) or by any concern which would not qualify as a small business concern under 37 CFR 1.9(d) or a nonprofit organization under 37 CFR 1.9(e).

*NOTE: Separate verified statements are required from each named person, concern or organization having rights to the invention averring to their status as small entities. (37 CFR 1.27)

NAME		
ADDRESS		_
	•	
[] INDIVIDUAL	[] SMALL BUSINESS CONCERN	[] NONPROFIT ORGANIZATION

I acknowledge the duty to file, in this application or patent, notification of any change in status resulting in loss of entitlement to small entity status prior to paying, or at the time of paying, the earliest of the issue fee or any maintenance fee due after the date on which status as a small entity is no longer appropriate. (37 CFR 1.28(b))

I hereby declare that all statements made herein of my own knowledge are true and that all statements made on information and belief are believed to be true; and further that these statements were made with the knowledge that willful false statements and the like so made are punishable by fine or imprisonment, or both, under section 1001 of Title 18 of the United States Code, and that such willful false statements may jeopardize the validity of the application, any patent issuing thereon, or any patent to which this verified statement is directed.

Date: 1/1.5-98

Dennis Green Vice President

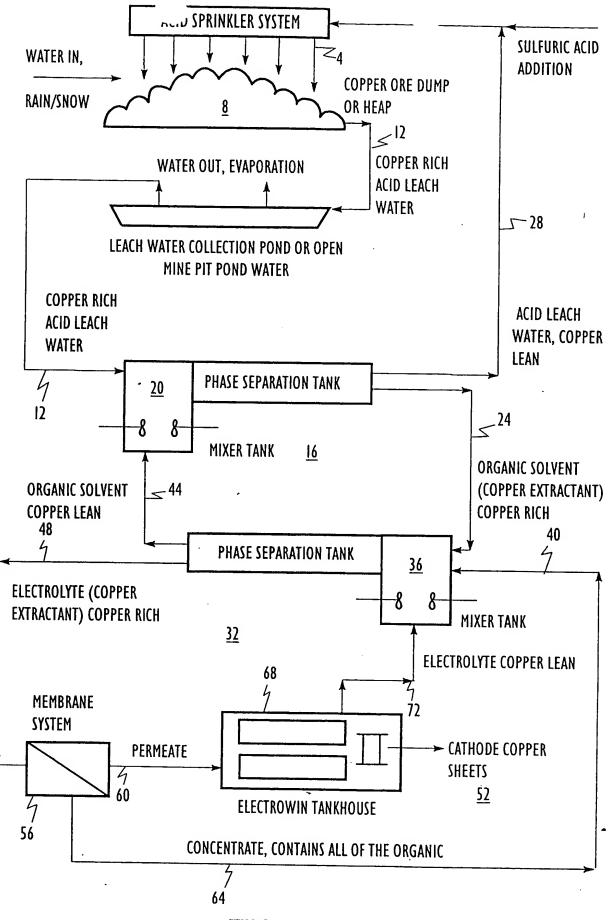


FIG. 1





IN THE UNITED STATES PATENT AND TRADEMARK OFFICE

#4

PATENT

In Re the Application of:

LOMBARDI

Serial No.: 60/099,717

Filed: September 10, 1998

Atty. File No.: 3376-21PROV2

For: "METHOD OF REMOVING

ORGANIC LIXIVIANT FROM COPPER SX-EW ELECTROLYTE

STREAM"

Assistant Commissioner for Patents Washington, D.C. 20231

Group Art Unit:

Examiner:

BY:

REQUEST FOR REFUND UNDER 37 CFR 1.26

CERTIFICATE OF MAILING

I HEREBY CERTIFY THAT THIS CORRESPONDENCE IS BEING DEPOSITED WITH THE UNITED STATES POSTAL SERVICE AS FIRST CLASS MAIL IN AN ENVELOPE ADDRESSED TO THE ASSISTANT COMMISSIONER OF PATENTS, WASHINGTON, DC 20231 ON January 12, 1999,

SHERIDAN ROSS 1

Dear Sir:

In connection with the filing of the above-identified U.S. patent application, Applicant hereby requests a refund in the amount of \$75.00. When the application was filed, the filing fee submitted was \$75.00. When the Notice to File Missing Parts (copy attached) was submitted to the Patent Office on November 12, 1998, an additional \$75.00 was paid along with the "Verified Statement (Declaration) Claiming Small Entity Status" signed by Dennis Green of HW PROCESS TECHNOLOGIES, INC. Accompanying this "Request for Refund" is a Small Entity Verification, the assignee of the aboveidentified application. In light of the filing of this Small Entity Declaration in a timely manner, it is respectfully submitted that small entity status should be accorded the application and,

therefore, the filing fee should be \$75.00 that was originally paid to the Patent Office.

It is respectfully requested that the overpayment of \$75.00 be tendered with for the Submission of Missing Parts, be returned by check made payable to the below-listed firm, on behalf of the assignee.

Respectfully submitted,

SHERIDAM ROSS P.C.

Bv:

Douglas W. Swartz

Registration No. 37,739

1700 Lincoln Street, Suite 3500

Denver, Colorado 80203

(303) 863-9700

Date:

PATENT APPLICATION

IN THE UNITED STATES PATENT AND TRADEMARK OFFICE

JAN 1 9 1999

In Re the Application of:

Group Art Unit:

LOMBARDI

Examiner:

Serial No.: 60/099,717

SUBMISSION OF MISSING

Filed: September 10, 1998

CERTIFICATE OF MAILING

Atty. File No.: 3376-21PROV2
For: "METHOD OF REMOVING

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COPPER SX-EW ELECTROLYTE

ORGANIC LIXIVIANT FROM

DC 20231 ON November 12, 1998.

STREAM"

AHERIDAN ROSS

Assistant Commissioner For Patents | Box Missing Part

Washington, D.C. 20231

Dear Sir:

In response to the Notice to File Missing Parts dated October 6, 1998, in connection with the above-identified application, enclosed herewith please find a Small Entity Statement. Please note that the Assignment documents have been submitted to the Assignment Branch under separate cover on this same date.

Also enclosed please find a check for \$100 which includes payment of the filing fee in the amount of \$75.00 reflecting small entity status, and the amount of \$25.00 payment of the surcharge. Please credit any overpayment or debit any underpayment to Deposit Account No. 19-1970. A copy of the Notice to File Missing Parts is also enclosed.

Please address all future correspondence to the undersigned attorney at the address below.

Respectfully submitted,

SHERIDAN ROSS P.C.

Douglas W. Swartz C Registration No. 37,739

1700 Lincoln Street, Suite 3500

Denver, Colorado 80203

(303) 863-9700

Date: Nov. 12, 1998





UNITED STATES DEPARTMENT OF COMMERCE Patent and Trademark Office

Address: COMMISSIONER OF PATENTS AND TRADEMARK
Washington, D.C. 20231

APPLICATION NUMBER 78 TRANSFILING/RECEIPT DATE FIRST NAMED APPLICANT ATTORNEY DOCKET NO/TITLE

60/099,717

09/10/98

FOREEN

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3376-21FR0V2

0242/1006

DOUGLAS W SWARTZ SHERICAN ROSS 1700 LINCOLN STREET SUITE 3500 DENVER CO 80203 MOT ASSIGNED,

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DATE MAILED:

10/08/98

NOTICE TO FILE MISSING PARTS OF PROVISIONAL APPLICATION Filed Under 37 CFR 1.53(c) No Filing Date (Enclosure to Form PTO-1626)

The required items noted below SHOULD be filed along with any items required on the "Notice of Incomplete Provisional Application." The filing date of this PROVISIONAL APPLICATION will be the date of receipt of the items required on the "Notice of Incomplete Provisional Application." The items noted below must be filed no later than TWO MONTHS FROM THE FILING DATE ACCORDED THIS APPLICATION. If Items 1 or 2 below are submitted after the filing date accorded this application, the SURCHARGE set forth in 37 CFR 1.16(I) of \$\square\$ \$25.00 for a small entity in compliance with 37 CFR 1.27, or \$\square\$ \$50.00 for a non-small entity, must also be timely submitted in reply to this NOTICE to avoid abandonment.

If all required items on this form and on the "Notice of Incomplete Application" are filed together, the total amount owed by applicant as a small entity (statement filed) non-small entity is \$______.

1. The statutory provisional application filing fee is:
 ______ missing.
 _______ insufficient.
 ________ to complete the basic filing fee and/or file a small entity statement claiming such status (37 CFR 1.27).

- The provisional application cover sheet under 37 CFR 1.51(c)(1) is required identifying:
 either the city and state or city and foreign country of the residence of each inventor.
 the title of the invention.
- ☐ 3. The application was filed in a language other than English.

 Applicant must file an English translation of the application, the \$130.00 set forth in 37 CFR 1.17(K),unless previously submitted, and a statement that the translation is accurate (37 CFR 1.52 (d)).
- ☐ 4. A \$50.00 processing fee is required since your check was returned without payment (37 CFR 1.21(m)).
- ☐ 5. Your filing receipt was mailed in error because your check was returned without payment.
- ☐ 6. The drawings contained in the application cannot be scanned or properly stored because they:
 ☐ do not comply with the size requirements (8 1/2 by 11 inches or 21.0 by 29.7 cm)
- are not clear enough or in permanent ink.
- The specification cannot be scanned or properly stored. Page(s)

do not contain writing on only one side of the page.

do not comply with the size requirements (8 1/2 by 11 inches or 21.0 by 29.7 cm).

are not clear enough or in permanent ink.

Replacement pages, together with a statement that the replacement page(s) contain no new matter, are required.

8. Other: _____

Direct the reply and any questions about this notice to "Attention: Box Missing Parts."

A copy of this notice <u>MUST</u> be returned with the reply.

PTO-103P

(Rev. 8-95) PROVISIONAL APPLICATION FILING RECEIPT CORRECTED



UNITED STATES DEPARTMENT OF COMMERCE Patent and Trademark Office ASSISTANT SECRETARY AND COMMISSIONER OF PATENTS AND TRADEMARKS Washington, D.C. 20231

APPLICATION NUMBER **FILING DATE**

FIL FEE REC'D ATTORNEY DOCKET NO DRWGS

60/099,717 09/10/98

\$175.00 3376-21PROV2

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DOUGLAS W SWARTZ SHERIDAN ROSS 1700 LINCOLN STREET **SUITE 3500** DENVER CO 80203

JAN 1 9 1999

RECEIVED

DEC 14 1998;

SHERIDAN ROSS PC

Receipt is acknowledged of this Provisional Application. This Provisional Application will not be examined for patentability. Be sure to provide the PROVISIONAL APPLICATION NUMBER, FILING DATE, NAME OF APPLICANT, and TITLE OF INVENTION when inquiring about this application. Fees transmitted by check or draft are subject to collection. Please verify the accuracy of the data presented on this receipt. If an error is noted on this Filing Receipt, please write to Box Provisional Application within 10 days of receipt. Please provide a copy of the Provisional Application Filing Receipt with the changes noted thereon. This Provisional Application will not be subject to review to pending status become date which is after twolve (12) months after its filing date and will not be subject to review to pending status become date which is after twolve (13) months. after its filing date and will not be subject to revival to restore it to pending status beyond a date which is after twelve (12) months from its filing date.

Applicant(s)

DENNIS H. GREEN, ARVADA, CO; JEFF MUELLER, BOULDER,

FOREIGN FILING LICENSE GRANTED 09/28/98 TITLE

SMALL ENTITY *

METHOD OF REMOVING ORGANIC LIXIVIANT FROM COPPER SX-EW ELECTROLYTE STREAM

DATA ENTRY BY: YON, LOWUAN

TEAM: 05 DATE: 12/08/98

SERIAL NUMBER		FILING DATE	CLASS	GROUP ART UNIT	ATTORNEY DO	CKET NO.	
60/099, PROVISIO		09/10/98		0000	3376-21P	ROV2	
APPLICANT DENUIS H.	GREEN, ARVA	DA, CO; JEFF	MUELLER, BOULD	ER, CO.			
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371 (NAT	T'L STAGE) D	ATA*****	*****				
FOREIGN VERIFIED	APPLICATIONS	S********					
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FOREIGN FI	LING LICENSE	E GRANTED 09/2	28/98 *	**** SMALL ENTI	TY ****		
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DOUGLAS W SHERIDAN 1700 LINC SUITE 350 DENVER CO	ROSS OLN STREET O	Initials Initia	,				
METHOD OF STREAM	REMOVING OR	GANIC LIXIVIA	NT FROM COPPER	SX-EW ELECTRO	LYTE		
FILING FEE RECEIVED \$175	No to charge/credit DEPOSIT ACCOUNT NO for the following: 1.16 Fees (Filing) 1.17 Fees (Processing Ext. of time) 1.18 Fees (Issue)						
				Other Credit			

PATENT APPLICATION

IN THE UNITED STATES PATENT AND TRADEMARK OFFICE

In Re the Application of:

LOMBARDI

Serial No.: 60/099,717

Filed: September 10, 1998

Atty. File No.: 3376-21PROV2

For: "METHOD OF REMOVING

ORGANIC LIXIVIANT FROM COPPER SX-EW ELECTROLYTE

STREAM"

Assistant Commissioner For Patents

Box Missing Part

20231 Washington, D.C.

Group Art Unit:

Examiner:

SUBMISSION OF MISSING PARTS

CERTIFICATE OF MAILING

I HEREBY CERTIFY THAT THIS CORRESPONDENCE IS BEING DEPOSITED WITH THE UNITED STATES POSTAL SERVICE AS FIRST CLASS MAIL IN AN ENVELOPE ADDRESSED TO ASSISTANT COMMISSIONER FOR PATENTS, WASHINGTON,

DC 20231 ON November 12, 1998.

&HĖRIDAN ROSS 🛧

Dear Sir:

In response to the Notice to File Missing Parts dated October 6, 1998, in connection with the above-identified application, enclosed herewith please find a Small Entity Statement. Please note that the Assignment documents have been submitted to the Assignment Branch under separate cover on this same date.

Also enclosed please find a check for \$100 which includes payment of the filing fee in the amount of \$75.00 reflecting small entity status, and the amount of \$25.00 payment of the surcharge. Please credit any overpayment or debit any underpayment to Deposit "Account No. 19-1970. A copy of the Notice to File Missing Parts is also enclosed.

Please address all future correspondence to the undersigned attorney at the address below.

Respectfully submitted,

SHERIDAN ROSS P.C.

By:

Dougkas W. Swartz

Registration No. 37,739

1700 Lincoln Street, Suite 3500 Denver, Colorado 80203 (303) 863-9700

Date: Nov. 12, 1998

RIFIED STATEMENT (DECLARATION) CLAIMING SMALL ENTITY STATUS (37 CFR 1.9(f) and 1.27(c)) - SMALL BUSINESS CONCERN

I herebyædeclare that I am an official empowered to act on behalf of the small business concern, HW PROCESS TECHNOLOGIES, INC. of 1208 Quail Street, Lakewood, Colorado 80215.

I hereby declare that the above-identified small business concern qualifies as a small business concern as defined in 13 CFR 121.3-18, and reproduced in 37 CFR 1.9(d), for purposes of paying reduced fees under section 41(a) and (b) of Title 35, United States Code, in that the number of employees of the concern, including those of its affiliates, does not exceed 500 persons. For purposes of this statement, (1) the number of employees of the business concern is the average over the previous fiscal year of the concern of the persons employed on a full-time, part-time or temporary basis during each of the pay periods of the fiscal year, and (2) concerns are affiliates of each other when either, directly or indirectly, one concern controls or has the power to control both.

I hereby declare that rights under contract or law have been conveyed to and remain with the small business concern identified above with regard to the invention, entitled "METHOD OF REMOVING ORGANIC LIXIVIANT FROM COPPER SX-EW ELECTROLYTE STREAM" and identified as Attorney File No. 3376-21PROV2, described in application Serial No. 60/099,717, filed on September 10, 1998.

If the rights held by the above-identified small business concern are not exclusive, each individual, concern or organization having rights to the invention is listed below* and no rights to the invention are held by any person, other than the inventor, who could not qualify as a small business concern under 37 CFR 1.9(c) or by any concern which would not qualify as a small business concern under 37 CFR 1.9(d) or a nonprofit organization under 37 CFR 1.9(e).

*NOTE: Separate verified statements are required from each named person, concern or organization having rights to the invention averring to their status as small entities. (37 CFR 1.27)

NAME							
ADDRESS							
[] INDIVIDUAL	[] SMALL BUSINESS CONCERN	[] NONPROFIT ORGANIZATION					

I acknowledge the duty to file, in this application or patent, notification of any change in status resulting in loss of entitlement to small entity status prior to paying, or at the time of paying, the earliest of the issue fee or any maintenance fee due after the date on which status as a small entity is no longer appropriate. (37 CFR 1.28(b))

I hereby declare that all statements made herein of my own knowledge are true and that all statements made on information and belief are believed to be true; and further that these statements were made with the knowledge that willful false statements and the like so made are punishable by fine or imprisonment, or both, under section 1001 of Title 18 of the United States Code, and that such willful false statements may jeopardize the validity of the application, any patent issuing thereon, or any patent to which this verified statement is directed.

Date: 11-5-98

Dennis Green
Vice President





UNITED STATES DEPARTMENT OF COMMERCE Patent and Trademark Office

Address: COMMISSIONER OF PATENTS AND TRADEMARK Washington, D.C. 20231

APPLICATION NUMBER	FILING/RECEIPT I	DATE	FIRST NAMED APPLICANT	ATTO	PRNEY DOCKET NO./TITLE
60/099,717	99 10,98	FORKEN		1	937A-21FRC

0242/1006

DOUGLAS W SWARTZ SHERIDAN ROSS 1700 LINCOLN STÉEET SUITE 3500 DENVER CO 80203

NOT ASSIGNED

*U.S. GPO: 1997-434

0000

DATE MAILED:

10/06/98

NOTICE TO FILE MISSING PARTS OF PROVISIONAL APPLICATION Filed Under 37 CFR 1.53(c)

No Filing Date (Enclosure to Form PTO-1626)

The required items noted below SHOULD be filed along with any items required on the "Notice of Incomplete Provisional Application." The filing date of this PROVISIONAL APPLICATION will be the date of receipt of the items required on the "Notice of Incomplete Provisional Application." The items noted below must be filed no later than TWO MONTHS FROM THE FILING DATE ACCORDED THIS APPLICATION. If items 1 or 2 below are submitted after the filing date accorded this application, the SURCHARGE set forth in 37 CFR 1.16(I) of \$25.00 for a small entity in compliance with 37 CFR 1.27, or \$50.00 for a non-small entity, must also be timely submitted in reply to this NOTICE to avoid abandonment.

If all required items on this form and on the "Notice of Incomplete Application" are filed together, the total amount owed by applicant as a □ small entity (statement filed) □ non-small entity is \$	
The statutory provisional application filing fee is: missing. insufficient. Applicant must submit \$ to complete the basic filing fee and/or file a small entity statement claiming such status (37 CFR 1.27).	
 The provisional application cover sheet under 37 CFR 1.51(c)(1) is required identifying: either the city and state or city and foreign country of the residence of each inventor. the title of the invention. 	
The application was filed in a language other than English. Applicant must file an English translation of the application, the \$130.00 set forth in 37 CFR 1.17(K), unless previously submitted, and a statement that the translation is accurate (37 CFR 1.52 (d)).	
4. A \$50.00 processing fee is required since your check was returned without payment (37 CFR 1.21(m)).	
5. Your filing receipt was mailed in error because your check was returned without payment.	
 ☐ 6. The drawings contained in the application cannot be scanned or properly stored because they: ☐ do not comply with the size requirements (8 1/2 by 11 inches or 21.0 by 29.7 cm) ☐ are not clear enough or in permanent ink. 	٠
☐ 7. The specification cannot be scanned or properly stored. Page(s)	
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8. Other:	
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Direct the reply and any questions about this notice to "Attention: Box Missing Parts." A copy of this notice MUST be returned with the reply. Customer Service Center	

Initial Patent Examination Division (703) 308-1202



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Address: COMMISSIONER OF PATENTS AND TRADEMARK Washington, D.C. 20231

APPLICATION NUMBER FILING/RECEIPT DATE FIRST NAMED APPLICANT ATTORNEY DOCKET NO//TITLE

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DATE MAILED:

NOTICE TO FILE MISSING PARTS OF PROVISIONAL APPLICATION

Filed Under 37 CFR 1.53(c) No Filing Date (Enclosure to Form PTO-1626)

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	donment.
If all r owed	required items on this form and on the "Notice of Incomplete Application" are filed together, the total amount by applicant as a \square small entity (statement filed) \square non-small entity is \$
	The statutory provisional application filing fee is: insufficient. Applicant must submit \$ to complete the basic filing fee and/or file a small entity statement claiming such status (37 CFR 1.27).
□ 2.	The provisional application cover sheet under 37 CFR 1.51(c)(1) is required identifying: ightharpoonup either the city and state or city and foreign country of the residence of each inventor. ightharpoonup the title of the invention.
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□ 7.	The specification cannot be scanned or properly stored. Page(s)
	do not contain writing on only one side of the page.
	do not comply with the size requirements (8 1/2 by 11 inches or 21.0 by 29.7 cm).
•	are not clear enough or in permanent ink.
	Replacement pages, together with a statement that the replacement page(s) contain no new matter, are required.
8	. Other:
Direc	ct the reply and any questions about this notice to "Attention: Box Missing Parts."
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	\mathcal{L} A copy of this notice <u>MUST</u> be returned with the reply.

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Initial Patent Examination Division (703) 308-1202

PTO/SERS (11-95)

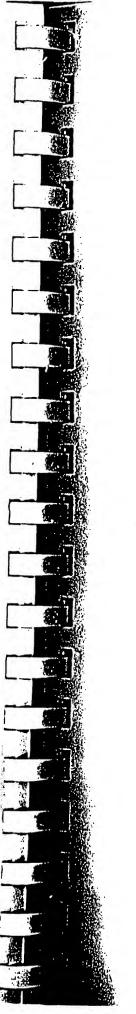
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Assistant Commissioner for Patents Washington, DC 20231	
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(A) referred to in United States Patent (B) referred to in an application that is Application No. paper number (C) an application that claims the sen Inspection, i.e., Application No. (D) an application in which the applica-	4(a)(3)(iv) to the application file record of the aboverage (CHECK ONE) Number 6/6/86 column sopen to public inspection as set form in 37 CFR 1.11, i.e., on page of on page of effect of the filing sate of an application that is open to public filed or of entitions an application to lay open the complete of entity this recuest to the following appress:
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JS006156186A

United States Patent [19]

Mueller et al.

[11] Patent Number:

6,156,186

[45] Date of Patent:

*Dec. 5, 2000

[54] METHOD FOR REMOVING CONTAMINANTS FROM PROCESS STREAMS IN METAL RECOVERY PROCESSES

[75] Inventors: Jeff Mueller, Boulder; Dennis H.

Green, Arvada, both of Colo.

[73] Assignee: HW Process Technologies, Inc.,

Lakewood, Colo.

[*] Notice: This patent is subject to a terminal dis-

claimer.

[21] Appl. No.: 09/183,683

[22] Filed: Oct. 30, 1998

Related U.S. Application Data

[60] Provisional application No. 60/100,510, Sep. 16, 1998, provisional application No. 60/100,494, Sep. 16, 1998, provisional application No. 60/077,878, Mar. 13, 1998, provisional application No. 60/074,428, Mar. 9, 1998, provisional application No. 60/064,284, Oct. 30, 1997, provisional application No. 60/064,279, Oct. 30, 1997, provisional application No. 60/099,717, Sep. 10, 1998, and provisional application No. 60/100,497, Sep. 16, 1998.

[56]

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(List continued on next page.)

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Eriksson et al., "Nanofiltration for Removal of Surplus Water in Dump Leaching", *Tailings and Mine Waste '96* Conference, Colorado State University Ft. Collins, Jan. 16–19, 1996, pp. 1–7.

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"Pilot Plant Studies on the Relationship between Copper Solvent Extraction Reagents and Crud Formation": Society for Mining, Metallurgy, and Exploration, Inc.; Preprint No. 96-35; Mar. 11-14, 1996; pps. 1-5.

"Cross Contamination of ODC Solvent Extraction Circuits"; Society for Mining, Metallurgy, and Exploration, Inc.; Preprint No. 96-162; Mar. 11-14, 1996; pps. 1-10.

(List continued on next page.)

Primary Examiner—Donald R. Valentine Attorney, Agent, or Firm—Sheridan Ross P.C.

[57] ABSTRACT

The present invention is directed to a process for removing various contaminants (e.g., organic collectors, contaminant metals or spectator ions, and/or suspended and colloidal solids) from process streams in leaching processes. The contaminant removal is performed by one or more membrane filtration systems (e.g., nanofilters, ultrafilters, and/or microfilters) treating process streams including, the pregnant leaching solution, the barren raffinate, and the lean and rich electrolytes.

33 Claims, 7 Drawing Sheets

